

1       **A PROCESS FOR SAFELY DECONTAMINATING THE CHILL WATER**  
2                   **USED IN MEAT PROCESSING**  
3

4       **CROSS REFERENCE TO RELATED APPLICATIONS AND CLAIM TO PRIORITY**  
5

6       This application is a continuation-in-part application of provisional application Serial  
7       No. 60/421,643 filed on October 28, 2002, the contents of which are hereby  
8       incorporated into this application. This application claims the benefit of provisional  
9       application Serial No. 60/421,643 filed on October 28, 2002.

10       **BACKGROUND OF THE INVENTION**  
11

12  
13       1.       Field of the Invention

14       This invention relates to a process for safely decontaminating the chill water used in  
15       meat processing. The decontaminant used in the process is chlorine dioxide.

16  
17       2.       Description of the Prior Art

18       Freshly slaughtered poultry or other meat products are contaminated with pathogenic  
19       microorganisms. These microorganisms are present both on the surfaces of the animals,  
20       as well as in the intestinal tracts immediately after slaughter or evisceration. To insure  
21       product safety, recent federal regulations require microbiological testing rather than  
22       visual inspection. These regulations require that carcasses be tested for *Salmonella*.

23  
24       A number of processes, which employ biocides for the pathogen control, have been  
25       proposed to decontaminate the chill water used to process poultry and other meat  
26       products. These processes include the use of chlorine-based sanitizers, chlorine dioxide,  
27       acidified sodium chlorite solutions, ozone and peracetic acid, but there are problems  
28       associated with using these chemicals. Ozone has poor persistence, while peracetic acid  
29       is only effective in high doses. Chlorine based sanitizers are inexpensive, but are less  
30       effective particularly at higher chill water pH. Chlorine dioxide is more effective, but  
31       can create health problems for workers exposed to it.

32  
33       U.S. Patent 5,389,390 suggests a process for removing bacteria from poultry, which  
34       involves using aqueous solution containing about 0.001% to about 0.2% by weight of a

1 metal chlorite, such that the chlorite ion is in the form of chlorous acid. While this  
2 process is capable of controlling some of the microorganisms in the chill water, it does  
3 not provide flexibility with respect to adjusting the feed rate of metal chlorite to the  
4 process water being treated as the demand of the treated water increases. In addition,  
5 chlorous acid is not as effective in reducing pathogenic organisms such as salmonella  
6 and E. coli.

7  
8 U.S. Patent 5,227,306 suggests a process and apparatus that provide flexibility for  
9 adjusting the feed and feed rate of chlorine dioxide to an aqueous system. The chlorine  
10 dioxide is generated on-site by an external generator, and the feed and feed rate are  
11 automatically controlled by means of a multiple feedback loop system. This process  
12 provides adequate oxidative treatment while avoiding overfeed or underfeed conditions.  
13 However, the applications described in the patent do not relate to systems where food  
14 and people are exposed to the chlorine dioxide, and does disclose the use of an air  
15 monitoring system, which would shut down the unit should vapor levels exceed defined  
16 limits.

17  
18 U.S. Patent 5,635,231 suggests a process for treating poultry and red meat that removes,  
19 retards, or reduces bacterial growth. The processes involve spraying the meat, either  
20 prior to or after introducing the meat into the chiller, with a solution of trialkali metal  
21 phosphate to decontaminate the meat. One of the problems with this process is that  
22 high amounts of the phosphate are used, which are discharged into the environment.  
23 U.S. Patent 5,700,507 teaches that the discharge can be minimized if the trialkali metal  
24 phosphate is used in conjunction with a steam treatment.

25  
26 U.S. Patent 5,683,724 describes an automated process for inhibiting microbial growth  
27 in aqueous food transport or process streams. In this process, a percarboxylated acid,  
28 such as peracetic acid, is used as the microbiological control agent. The amount of  
29 percarboxylated acid fed is controlled by maintaining an ORP between 280 and 460  
30 mV. The patent notes that the use of chlorine dioxide is undesirable, because it is a  
31 toxic gas and has an acceptable air concentration limit of 0.1 ppm. Exposure to levels  
32 above this amount may cause headaches, nausea, and respiratory problems. The patent

1 goes on to note that expensive and intricate safety devices and/or equipment are needed  
2 when using chlorine dioxide as a decontaminant, in order to monitor the level of  
3 chlorine dioxide and maintain concentrations below 0.1 ppm. The art described in the  
4 invention addresses these concerns and provides a solution in a safe manner.

5  
6 Clearly, there is a need in the meat processing industry for a process that effectively  
7 decontaminates the meat as well as the process water, which does not damage the meat  
8 being treated, and also insures the safety of workers connected with the treatment  
9 process.

10  
11 All citations referred to under this description of the "Related Art" and in the "Detailed  
12 Description of the Invention" are expressly incorporated by reference.

#### 13 14 BRIEF SUMMARY OF THE INVENTION

15  
16 This invention relates to a process for safely decontaminating the chill water used in  
17 meat processing. The process is carried out once an operational signal, which is  
18 monitored, is received from the poultry chill system indicating that there is chill water  
19 in the chill bath. The process comprises:

- 20
- 21 (a) measuring the oxidative-reduction potential of the chill water in the chill  
22 bath of the chiller, preferably with an oxidative-reduction potential  
23 sensor, prior to introducing the meat to be processed and chlorine  
24 dioxide into the chill water, in order to obtain a reference oxidative-  
25 reduction potential for said chill water,
  - 26
  - 27 (b) introducing the meat to be processed into the chill water,
  - 28
  - 29 (c) feeding chlorine dioxide, preferably an aqueous solution of chlorine  
30 dioxide, to said chill water to achieve a predetermined target oxidative-  
31 reduction potential in the chill water from between 400 mV to 750 mV,

1 more preferably from 475 mV to 700, and most preferably from 580 mV  
2 to 680 mV,

3  
4 wherein said chlorine dioxide is preferably generated on site by  
5 means of a chlorine dioxide generator achieving a generation  
6 efficiency of at least 90%,

7  
8 wherein the concentration of chlorine dioxide fed is from 100  
9 ppm to 3000 ppm, preferably of 750 ppm to 2000 ppm, and

10  
11 wherein the amount of chlorine dioxide fed is sufficient to  
12 increase the oxidative-reduction potential of the chill water to a  
13 level that exceeds the reference oxidative-reduction potential  
14 established in (a), and achieves the target oxidative-reduction  
15 potential referenced in (c), provided that the level of chlorine  
16 dioxide in the chill water does not exceed a residual level of 3.0  
17 ppm;

18  
19 (d) monitoring the oxidative-reduction potential of the chill water;

20  
21 (e) monitoring the level of chlorine dioxide gas in the atmosphere  
22 surrounding the chill water; and

23  
24 (f) terminating the flow of chlorine dioxide into the chill water, if the  
25 oxidative-reduction potential exceeds 750 mV, if the oxidative-reduction  
26 potential of the chill water meets the target established in (c), or if the  
27 level of chlorine dioxide gas in the atmosphere surrounding the chill  
28 water exceeds 0.3 ppm., preferably 0.25 ppm.

29  
30 The process described herein effectively decontaminates the chill water used in  
31 processing poultry, does not damage the meat treated, and insures the safety of workers  
32 connected with the treatment process.

1  
2 BRIEF DESCRIPTION OF THE SEVERAL VIEWS OF THE DRAWINGS  
3

4 Figure 1 is drawing that shows the equipment used in the process for decontaminating  
5 the chill water used in processing poultry.  
6

7 DETAILED DESCRIPTION OF THE INVENTION

8 For purposes of this invention, “meat” means animal protein derived from beef, lamb,  
9 poultry, seafood, and the like, most typically poultry and seafood.  
10

11 Any chiller that contains a chilled water bath to chill the meat carcasses can be used.  
12 Although in some chillers, the chilled water bath is not circulated, i.e., the water either  
13 remains in the chiller or is used one time only and discharged, typically the chiller re-  
14 circulates the chilled water. When processing meat for human consumption, it is  
15 necessary that the slaughtered, eviscerated meat carcasses be chilled as rapidly as  
16 possible.  
17

18 Examples of chillers include “drag type chillers”, as disclosed in U.S. Patent 4,788,831  
19 and “auger-type chillers”, as disclosed in U.S. Patent 5,868,000.  
20

21 Before adding the meat to the chill water, the meat is scalded, eviscerated, cropped,  
22 boned, gutted, and/or degutted, and washed. In some cases, the meat is first treated  
23 with a trialkali phosphate, peracetic acid or acidified chlorite to help remove fecal  
24 matter and control *E. coli*. Chill water temperature varies and is typically set by plant  
25 requirements and good manufacturing practices, however, prechill water cannot exceed  
26 65° F while chill water is typically maintained below 40° F.  
27

28 For purposes of this invention, “chlorine dioxide” includes an aqueous solution of  
29 chlorine dioxide. Chlorine dioxide may be generated on-site using techniques and  
30 equipment well-known in the art. For instance, chlorine dioxide solution can be  
31 generated on-site using an alkali chlorite and chlorine gas; an alkali chlorite and  
32 hypochlorite with mineral acid or an alkali chlorate and mineral acid. Examples of  
33 generation equipment suitable for use in the process are described in U.S. Patents

1 4,013,761 and 4,147,115. Various means may be used to control the delivery of sodium  
2 chlorite and other chemicals to the generator. Such means include, but are not limited  
3 to, variable rate pumps, valves, eductors and metering devices. The chlorine dioxide is  
4 fed to the chill water at levels, so that residual levels do not exceed 3.0 ppm, and  
5 preferably is between 0.1 ppm to 0.5 ppm.

6  
7 The feed and feedrate of chlorine dioxide can be regulated by multiple, redundant  
8 oxidation-reduction (ORP) technology analyzers, sensors, and a Master Control Unit.  
9 See, for example, U.S. Patent 5,227,306, which describes how to proportionally feed  
10  $\text{ClO}_2$  to an aqueous system. Alternatively, it may also be fed through an on/off cycling  
11 mechanism based upon the ORP.

12  
13 The total control system consists of a Master Control Unit, which is a PLC  
14 (programmable logic controller)-based system comprising control logic and an operator  
15 interface. Any PLC and operator interface-based system can be used. The Master  
16 Control Unit regulates all aspects of feeding  $\text{ClO}_2$  to the chill water and provides a  
17 safety interlock to prevent overfeed of chlorine dioxide, so that effective operation is  
18 insured in a safe manner. The master control unit also initiates alarms, collects and  
19 stores critical operating data, and provides a means to download said data either  
20 remotely or locally. Remote download may be accomplished via telephone or cellular  
21 technology.

22  
23 The oxidative-reduction potential of the chill water is preferably measured with an  
24 oxidative-reduction potential sensor. Sensors, typically having probes, which are in  
25 direct contact with the chill water, are connected to the ORP analyzer. These sensors  
26 are in direct contact with the chill water. The primary ORP analyzer monitors the  
27 oxidative-reduction potential of the chill water and feeds the information to the Master  
28 Control Unit. The Master Control Unit then regulates the feed of chlorine dioxide to  
29 the meat chill water, based upon input from the ORP analyzer.

30  
31 The operation of ORP sensors is less than optimal, because of the presence of greasy  
32 poultry fat or skin, which can lodge against the probe of the sensor and coat the sensor.

1 This can result in readings that do not accurately reflect the oxidative state of the chill  
2 water, and cause an underfeed or overfeed of chlorine dioxide.

3  
4 To solve this problem, the process preferably uses two or more ORP analyzers and  
5 sensors, both of which monitor the chill water. The master controller continuously  
6 monitors and compares the two analyzers. If a discrepancy exists between the  
7 analyzers, which exceeds a preset limit, the master controller immediately initiates a  
8 probe wash. If the discrepancy remains after the probe wash, the unit automatically  
9 signals an alarm condition. This redundancy ensures continuous system control for  
10 reliability, safety, and pathogen control. In addition to a probe wash, a back flush of the  
11 probes with fresh water may be present and initiated in response to the conditions  
12 above.

13  
14 A primary safety feature of the design is an interlock design between the Master  
15 Control Unit and the operation of feeding the chlorine dioxide to the chill water from  
16 the chlorine dioxide generators. The Master Control Unit requires a signal from the  
17 chiller, indicating that there is water in the chiller, before the chlorine dioxide  
18 generators can begin feeding chlorine dioxide to the chill water. This signal could be  
19 detected from any number of mechanical, electrical or pneumatic devices that would  
20 indicate that a chiller is in operation such as valves, auger motors or chain motors.  
21 Preferably it would a signal from an ammonia refrigeration system through which the  
22 chill water flows and is typically obtained from a slip stream of water taken from the  
23 chill box, which is routed through the refrigeration system via a rechill pump or  
24 recirculating pump. The rechill pump or refrigeration system is preferably interlocked  
25 with the Master Control Unit. The interlock device insures that chill water is in place  
26 before chlorine dioxide is introduced to the chiller and it prevents the escape of airborne  
27 chlorine dioxide gas, which could pose a personnel hazard.

28  
29 Another feature of the ORP control function is the alarm system, which is activated at  
30 both high and low ORP levels. The low-level alarm is activated to notify personnel that  
31 insufficient oxidant residual may be present in the chill water, which could result in  
32 unacceptable levels of pathogenic bacteria. The high-level alarm is activated to notify

1 key personnel of the potential of exceeding upper regulatory limits for chlorine dioxide  
2 in the process water systems. Both process variables are monitored and alarms  
3 indicated by the Master Control Unit. The high level alarm will also suspend chlorine  
4 dioxide feed when the acceptable amount is exceeded.

5  
6 Another element of the process involves the use of chlorine dioxide-specific air quality  
7 monitors. The maximum air concentration limit for chlorine dioxide over an 8 hour  
8 period is 0.1 ppm. Exposure in excess to this level may lead to headaches, nausea, and  
9 respiratory problems and needs to be guarded against. Multiple chlorine dioxide-  
10 specific air quality monitors are incorporated into the system design and placed at key  
11 points around the immediate vicinity of the chillers. The monitors are placed at or  
12 above or below the chillers, typically 25 feet away, but preferable 5 to 10 feet away.  
13 Preferably, there is an electronic or electrical connection between the air monitors and  
14 the master controller so that output signals from the air monitor can pass to the Master  
15 Control Unit. In the event the air quality is unacceptable and exceeds preset limits of  
16 0.1 ppm (equivalent to the OSHA PEL), the master control unit will initiate an alarm.  
17 If the air quality exceeds a failsafe limit of 0.25 ppm (which we have selected to be just  
18 below the OSHA STEL), the master controller will terminate the flow of chlorine  
19 dioxide into the chill water and initiate a second alarm.

20  
21 The air quality monitors are connected to the Master Control Unit and continuously  
22 monitors air quality. As the monitor continuously samples the atmosphere, it provides a  
23 chlorine dioxide concentration readout locally, as well as remotely, through a 4-20 mA  
24 signal. If air quality deteriorates due to increasing levels of chlorine dioxide the Master  
25 Control Unit initiates an automatic shutdown of the chlorine dioxide generation system  
26 and automatically notifies key personnel. If air quality improves and contaminant levels  
27 fall below preset limits, the Master Control Unit initiates start-up of the chlorine  
28 dioxide generators and feed of oxidant will resume to the chill water.

## 30 ABBREVIATIONS AND DEFINITIONS

31 The following abbreviations are used in the Examples:



1		
2	GENEROX® generator	a chlorine dioxide generator that efficiently generates an
3		aqueous solution of chlorine dioxide in excess of 90% by
4		chlorine/chlorite, acid/hypochlorite/chlorite or acid/
5		chlorate sold by Drew Industrial Division, a division of
6		Ashland Specialty Chemical, a division of Ashland Inc.
7		
8	ONGUARD® IPC unit	an integrated pathogen master controller unit (IPC), (sold
9		by Drew Industrial, an operating business of Ashland
10		Specialty Chemical, a division of Ashland Inc.) that
11		monitors poultry chiller for operational signal, measures
12		and compares the oxidative-reduction potential of an
13		aqueous system in millivolts (mV), controls the operation
14		of GENEROX® chlorine dioxide generator, measures
15		and compares air quality, initiates alarms, and provides
16		for data collection and storage, as well as remote and
17		local data download capabilities.
18		
19	ORP	oxidative-reduction potential.
20		
21	ORP analyzer	measures oxidative-reduction potential in millivolts.
22		

## EXAMPLES

The examples will illustrate specific embodiments of the invention. These examples along with the written description will enable one skilled in the art to practice the invention. It is contemplated that many other embodiments of the invention will work besides these specifically disclosed. All parts are by weight and all temperatures are in °C unless otherwise specified. Controls or Comparative Examples are designated by letters.

### Example 1

1 The Master Control Unit requires a signal from the chiller, indicating that there is water  
2 in the chiller, before the chlorine dioxide generators begin pumping chlorine dioxide to  
3 the chill water. The signal typically is obtained from a slipstream of water taken from  
4 the chill box and routed through the refrigeration system via a rechill pump. The  
5 refrigeration system is interlocked with the Master Control Unit. The interlock device  
6 insures that chill water is in place before chlorine dioxide is introduced to the chiller  
7 and it prevents the escape of airborne chlorine dioxide gas, which could pose a  
8 personnel hazard.

9  
10 The signal indicating that the chiller is in operation is obtained before the poultry and  
11 chlorine dioxide are introduced into the chiller, and provides a reference point for the  
12 chill water. Initial chill water ORP reference point readings without poultry and  $\text{ClO}_2$   
13 present vary significantly. The reference point reading is below 400 mV, typically  
14 between -100 mV to +300 mV.

15  
16 If the ONGUARD IPC unit receives an indication that the chiller is in operation, it  
17 activates a GENEROX chlorine dioxide generator connected to chill box where the  
18 chill water is stored. If there is no signal to the ONGUARD IPC unit, the GENEROX  
19 generator is not activated, so that a potential personnel hazard is averted. In order to  
20 activate flow of chlorine dioxide from the GENEROX chlorine dioxide generator to the  
21 chill water, the ORP signal for the chill water must reach a level of from 400 mV to 750  
22 mV, most preferably from 580 mV to 680 mV.

23  
24 Processed poultry is introduced to the chill water of the chiller following carcass  
25 washing after is clear that the chiller is in operation and contains chill water in the chill  
26 box. The time the birds are transported through the chiller varies based upon the type,  
27 weight and starting temperature of the carcass.

28  
29 The introduction of the birds into the chill water results in decontamination of the chill  
30 water and causes the ORP to decrease. This decrease in ORP is recognized by the  
31 ONGUARD IPC unit, which activates a signal to the GENEROX generator to feed  
32  $\text{ClO}_2$  into the chill water. The ONGUARD IPC unit continuously measures the ORP of

1 the chill water, comparing it to the reference point. If the ORP of the chill water is  
2 below the reference point, the ONGUARD IPC unit signals the GENEROX generator  
3 to start feeding the aqueous solution of chlorine dioxide. The typical concentration of  
4 the aqueous solution of  $\text{ClO}_2$  is from 100 ppm to 3000 ppm, preferably 750 ppm to  
5 2,000 ppm.

6  
7  $\text{ClO}_2$  is fed directly to the chill water predominantly directly to the chill box, but also  
8 through the chill water recirculating line. As the chlorine dioxide is fed into the chill  
9 water, the ORP readings increase. Chlorine dioxide is fed to the chill water until the  
10 ORP readings achieve a preset limit, which indicates that the chill water has become  
11 decontaminated. Alternatively, the generator can proportion  $\text{ClO}_2$  to the system  
12 automatically based upon a pre-determined ORP level. Final ORP reading typically  
13 vary between 400 mV to 750 mV, preferably 580 mV and 680 mV, depending upon  
14 initial, pre-feed ORP, and system demand.

15  
16 When feeding the chlorine dioxide, the residual chlorine dioxide concentration in the  
17 chill water should not exceed 3 ppm residual  $\text{ClO}_2$ , but is typically targeted between 0.1  
18 ppm and 0.5 ppm.

19  
20 To prevent overfeed of chlorine dioxide, the ONGUARD IPC will initiate a shutdown  
21 of chlorine dioxide feed if the ORP exceeds a pre-designated set point. This prevents  
22 the system from exceeding regulatory chlorine dioxide limits. In a high ORP condition,  
23 the ONGUARD IPC will initiate an alarm condition. If chlorine dioxide were underfed,  
24 a low ORP would result. If the ONGUARD IPC detects this circumstance on either the  
25 primary analyzer, secondary analyzer or both, the unit would initiate a probe wash. If  
26 the low ORP condition continues to exist, then an alarm condition will activate. This  
27 helps ensure sufficient oxidant to control pathogens.

28  
29 The operating environment of the ORP sensors is less than optimal, because of the  
30 presence of greasy poultry fat or skin, which can lodge against the probe of the sensor  
31 and coat the sensor. This can result in a reading that does not accurately reflect the

1 oxidative state of the chill water, and causes an underfeed or overfeed of chlorine  
2 dioxide.

3

4 To solve this problem, the ONGUARD IPC preferably uses two ORP analyzers and  
5 sensors, both of which monitor the chill water. Preferably, the ONGUARD IPC  
6 continuously monitors and compares the two analyzers. If a discrepancy exists between  
7 the analyzers, which exceeds a preset limit, the ONGUARD IPC immediately initiates a  
8 probe wash. If the discrepancy remains after the probe wash, the unit automatically  
9 signals an alarm condition. This redundancy ensures continuous system control for  
10 reliability, safety, and pathogen control. This automatic probe wash is in addition to  
11 that triggered by low ORP detected on either analyzer as described above. In addition  
12 to the probe wash, a fresh water back flush of the probes may also be initiated.

13

14 During the operation of the system, the ONGUARD IPC system preferably  
15 continuously monitors air quality in the vicinity of the chill water systems using  
16 multiple chlorine dioxide specific air quality monitors. The monitors take continuous  
17 air measurements and send the result to the ONGUARD IPC. In the event the air  
18 quality is unacceptable and exceeds preset limits of 0.1 ppm [equivalent to the OSHA  
19 PEL (Permissible Exposure Limit)], an alarm will be initiated. If the air quality  
20 exceeds a failsafe limit of 0.25 ppm (which has determined to be just below the OSHA  
21 STELM (Short Term Exposure Limit), the ONGUARD IPC will initiate an automatic  
22 shutdown of the generating systems and initiate a second alarm. This is a key feature of  
23 the ONGUARD IPC and is a cornerstone of the safe introduction of chlorine dioxide  
24 into the chill water system.